

Calculating flow out of an open pipe using Bernoulli, Darcy-Weisbach

Bernoulli's Equation, solve for V_2 (ignoring height change component)

$$P_1 + \frac{1}{2} \cdot \rho \cdot v_1^2 = P_2 + \frac{1}{2} \cdot \rho \cdot v_2^2 \xrightarrow[\text{assume, } \rho > 0]{\text{solve, } v_2} \left[\begin{array}{c} \frac{\sqrt{\rho \cdot v_1^2 + 2 \cdot P_1 - 2 \cdot P_2}}{\sqrt{\rho}} \\ - \frac{\sqrt{\rho \cdot v_1^2 + 2 \cdot P_1 - 2 \cdot P_2}}{\sqrt{\rho}} \end{array} \right]$$

Flow Parameters

$$\rho_{\text{water}} := 1000 \frac{\text{kg}}{\text{m}^3} \quad \text{Water Density}$$

$$v_1 := 0 \frac{\text{m}}{\text{s}} \quad \text{Initial Velocity}$$

$$P_0 := 5 \text{ bar} \quad \text{Pressure at start of pipe}$$

$$P_1 := 1.33 \text{ bar} \quad \text{Pressure at pipe exit}$$

$$P_2 := 1 \text{ atm} \quad \text{Atmospheric Pressure}$$

$$C_D := 0.7 \quad \text{Discharge Coefficient}$$

$$D_{\text{orifice}} := 15 \text{ mm} \quad \text{Orifice Diameter}$$

$$A_{\text{orifice}} := \frac{\pi \cdot D_{\text{orifice}}^2}{4} = (1.767 \cdot 10^{-4}) \text{ m}^2 \quad \text{Calculate Pipe Exit Area}$$

Calculate discharge flow velocity at pipe exit (P.1 - P.2)

$$v_2 := C_D \cdot \frac{\sqrt{\rho_{\text{water}} \cdot v_1^2 + 2 \cdot P_1 - 2 \cdot P_2}}{\sqrt{\rho_{\text{water}}}} = 5.571 \frac{\text{m}}{\text{s}}$$

Calculate v_2 based on parameters
(takes into account discharge coefficient)

$$m_{\text{dot}} := v_2 \cdot A_{\text{orifice}} = 3.544 \frac{\text{m}^3}{\text{hr}}$$

Calculate m_{dot} based on flow rate

Estimate pipe head loss (P.0 - P.1):

Darcy-Weisbach equation:

$$\frac{\Delta P}{L} = f_D \cdot \frac{\rho_{fluid}}{2} \cdot \frac{v_{avg}^2}{D} \xrightarrow{\text{solve, } \Delta P} \frac{L \cdot f_D \cdot v_{avg}^2 \cdot \rho_{fluid}}{2 \cdot D}$$

Pipe flow parameters:

$$L := 20 \text{ m}$$

$$D := D_{orifice}$$

$$\nu_{water} := 1.052 \cdot 10^{-5} \frac{\text{ft}^2}{\text{s}} = (9.773 \cdot 10^{-7}) \frac{\text{m}^2}{\text{s}}$$

$$Re(v_{avg}) := \frac{v_{avg} \cdot D}{\nu_{water}} \quad Re(v_2) = 8.551 \cdot 10^4$$

$$f_D := 0.018 \quad f_D \text{ looked up in chart in EIT manual, smooth pipe, } Re = 8.5 \times 10^4$$

$$\rho_{fluid} := \rho_{water}$$

Solve for pressure drop:

$$\Delta P(v_{avg}) := \frac{L \cdot f_D \cdot v_{avg}^2 \cdot \rho_{fluid}}{2 \cdot D}$$

$$\Delta P_{itr} := \Delta P(v_2) = 3.725 \text{ bar}$$

$$\frac{\Delta P_{itr} + P_1}{P_0} = 1.011$$

Iterate P_1 and lookup "f" until in chart until $(P_1 + \Delta P = P_0)$

$$\Delta P_{itr} + P_1 = 5.055 \text{ bar}$$

Sum of P_1 and ΔP is close to original pressure of 5 bar