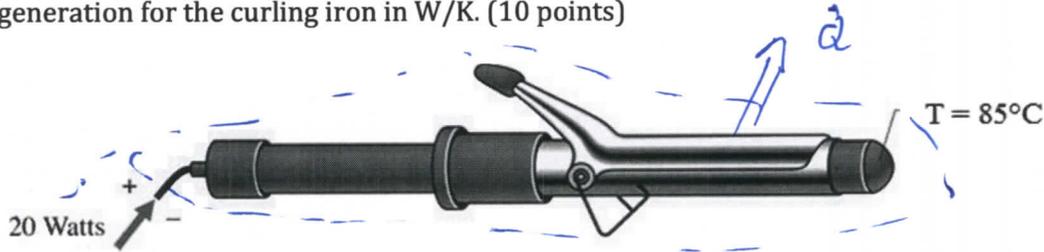


## Problems (Open Book)

1. A 20 W curling iron has a surface temperature of 85°C. Determine the rate of entropy generation for the curling iron in W/K. (10 points)



1<sup>st</sup> Law

$$0 = \dot{Q} - \dot{W}$$

$$\dot{W} = -20 \text{ W}$$

$$\dot{Q} = -20 \text{ W}$$

$$\frac{dE}{dt} = 0$$

2<sup>nd</sup> Law

$$0 = \frac{\dot{Q}}{T_b} + \dot{\sigma}$$

$$\frac{dS}{dt} = 0$$

$$\dot{\sigma} = -\frac{\dot{Q}}{T_b} = \frac{20 \text{ W}}{358 \text{ K}} = 0.0559 \frac{\text{W}}{\text{K}}$$

$$0 = -\dot{Q}_{out} + \dot{Q}_{in} + \dot{W}$$

2. A heat pump operating at steady-state maintains the inside of a building at 20°C while transferring heat from a well at 10°C. The heat pump transfers 120,000 kJ/h to the building. Over 14 days the heat pump consumes 1490 kW·h of electricity.
- (a) Find the amount of heat in kJ transferred from the well by the heat pump during the same 14 day period. (5 points)
- (b) What is the coefficient of performance for the heat pump? (5 points)
- (c) What is the maximum coefficient of performance for this heat pump when operating between the well (10°C) and the building (20°C)? (5 points)

$$(a) W_{cycle} = Q_{out} - Q_{in}$$

$$Q_{out} = 120,000 \frac{\text{kJ}}{\text{h}} \left( \frac{24\text{h}}{\text{day}} \right) 14 \text{ days} \\ = 40.32 \times 10^6 \text{ kJ}$$

$$W_{cycle} = 1490 \text{ kW}\cdot\text{h} \left( \frac{1 \text{ kJ/s}}{1 \text{ kW}} \right) \cdot \frac{3600 \text{ s}}{1 \text{ h}} = 5.364 \times 10^6 \text{ kJ}$$

$$Q_{in} = Q_{out} - W_{cycle} \\ = (40.364 - 5.364) \times 10^6 \text{ kJ} \\ = 34.956 \times 10^6 \text{ kJ}$$

$$(b) \beta_{HP} = \frac{Q_{out}}{W_{cycle}} = 7.52$$

$$(c) \beta_{HP, \max} = \frac{T_H}{T_H - T_C} = \frac{293 \text{ K}}{(293 - 283) \text{ K}} = 29.3$$

3. Nitrogen ( $N_2$ ) at 1 bar,  $37^\circ\text{C}$  is compressed to 10 bar using a well-insulated compressor. The mass flow rate is 1000 kg/h and the specific heat ratio of nitrogen is  $k = 1.391$ .
- (a) What is the minimum theoretical work needed to compress the gas? (10 points)
- (b) If the exit temperature of the compressor is  $397^\circ\text{C}$ , what is the isentropic efficiency of the compressor? (10 points)
- (c) Suppose the compressor is poorly insulated, but the exit temperature is still  $397^\circ\text{C}$ . Would the isentropic efficiency be higher or lower? Justify your answer using the 1st and 2nd Laws. (5 points)

$$(a) \dot{m}_1 = \dot{m}_2 \quad (1 \text{ in}, 1 \text{ out})$$

$$0 = \dot{Q} - \dot{W} + \dot{m}(h_1 - h_2)$$

$$\dot{W} = \dot{m} c_p (T_1 - T_2)$$

$$c_p = \frac{kR}{k-1} \quad R_{N_2} = \frac{8.314 \frac{\text{J}}{\text{mol}\cdot\text{K}}}{28 \frac{\text{g}}{\text{mol}}} = 0.2969 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$$

$$= \frac{1.391(0.2969) \frac{\text{kJ}}{\text{kg}\cdot\text{K}}}{0.391}$$

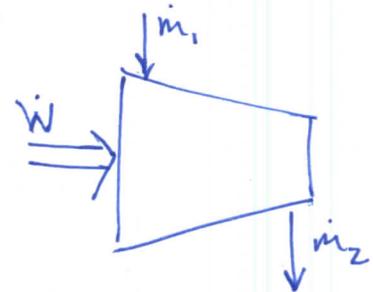
$$= 1.056 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$$

$$\dot{W}_s = \dot{m} c_p (T_1 - T_{2s})$$

$$T_{2s} = T_1 \left( \frac{P_2}{P_1} \right)^{\frac{k-1}{k}} = 310 \text{ K} (10)^{\frac{0.391}{1.391}} = 592.2 \text{ K}$$

$$\dot{W}_s = 1000 \frac{\text{kg}}{\text{h}} \left( \frac{1 \text{ K}}{3600 \text{ s}} \right) \left( 1.056 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \right) (310 - 592.2) \text{ K}$$

$$\dot{W}_s = -82.78 \text{ kW}$$



- ① Well-ins.
- ② Steady-state
- ③  $\Delta PE + \Delta KE \sim 0$
- ④ Ideal gas,  $c_p = \text{const.}$

$$(b) \dot{W} = \dot{m} c_p (T_1 - T_2)$$

$$= 1000 \frac{\text{kg}}{\text{h}} \left( \frac{1 \text{h}}{3600 \text{s}} \right) (1.056 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}) (310 - 670) \text{K}$$

$$= -105.6 \text{ kW}$$

$$\eta_c = \frac{\dot{W}_s}{\dot{W}} = 78.4\%$$

(c) If there is  $\dot{Q} \neq 0$  then

1st Law  ~~$\dot{W}$~~   $0 = \dot{Q} - \dot{W} + \dot{m} c_p (T_1 - T_2)$

2nd Law  $0 = \frac{\dot{Q}}{T_b} + \dot{m} \left[ c_p \ln\left(\frac{T_1}{T_2}\right) - R \ln\left(\frac{P_1}{P_2}\right) \right] + \dot{\sigma}$

$$0 = \frac{\dot{Q}}{T_b} + \dot{m} \left[ \frac{k}{k-1} \left( \frac{T_1}{T_2} \right) - \ln\left(\frac{P_1}{P_2}\right) \right] + \dot{\sigma}$$

$$-\dot{\sigma} = \frac{\dot{Q}}{T_b} + \dot{m} \left( 1000 \frac{\text{kg}}{\text{h}} \right) \left( 0.297 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} \right) \left( \frac{1 \text{h}}{3600 \text{s}} \right) \times \left[ \frac{1.391}{0.391} \ln\left(\frac{310}{670}\right) - \ln(0.1) \right]$$

$$\dot{\sigma} = -\frac{\dot{Q}}{T_b} + 0.0825 \left[ -0.43923 \right] \frac{\text{kW}}{\text{K}}$$

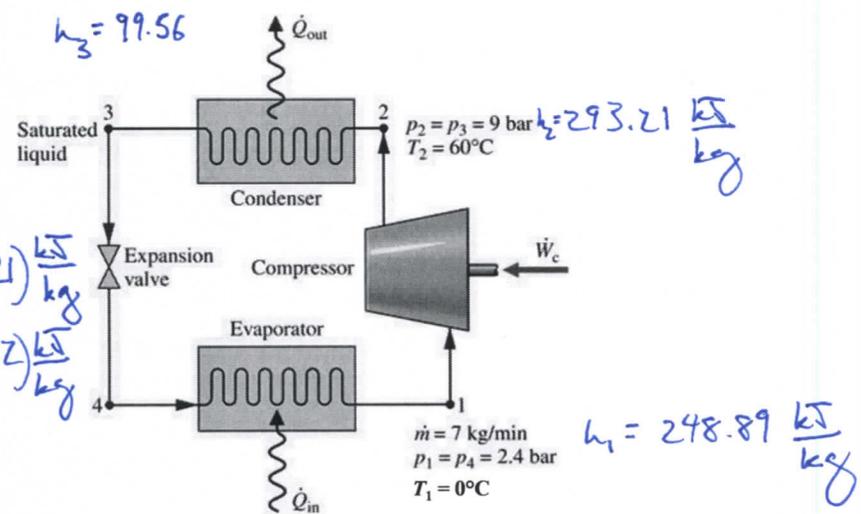
$\dot{\sigma} \geq 0$  + for non-ideal  $\dot{\sigma} > 0$

So  $\dot{Q} < 0$  (out) +  ~~$\dot{Q}$~~   $\frac{\dot{Q}}{T_b} < -0.0362 \frac{\text{kW}}{\text{K}}$

$\Rightarrow$   ~~$\dot{W} < -105.6$~~   $\dot{W}_{in}$  must be larger, so  $\eta_c$  will be smaller.

4. A heat pump using R-134a operates at steady-state as shown below.
- What is the work input into the compressor? (10 points)
  - What is the coefficient of performance for this heat pump? (10 points)
  - An inventor claims to have a turbine that can replace the expansion valve and recover 50% of the power required for the compressor. Is this a valid claim? Justify your answer with a number. (5 points)

(a)  $\dot{W}_c = \dot{m}(h_1 - h_2)$   
 $= \frac{7 \text{ kg}}{\text{min}} \frac{1 \text{ min}}{60 \text{ s}}$   
 $\times (248.89 - 293.21) \frac{\text{kJ}}{\text{kg}}$   
 $= 0.1167 \frac{\text{kg}}{\text{s}} (-44.32) \frac{\text{kJ}}{\text{kg}}$   
 $= -5.17 \text{ kW}$



(b)  $\beta_{HP} = \frac{\dot{Q}_{out}}{\dot{W}_c} = \frac{\dot{m}(h_2 - h_3)}{\dot{m}(h_1 - h_2)} = \frac{22.6 \text{ kW}}{5.17 \text{ kW}} = 4.37$

$\dot{Q}_{out} = \dot{m}(h_3 - h_2)$   
 $= -22.60 \text{ kW}$

(c) In a best case for the turbine

$s_{4s} = s_3 = 0.3656 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$  Sat. mixture at  $p_1$

$x_{4s} = \frac{s_{4s} - s_f}{s_g - s_f} = 0.259 \Rightarrow h_{4s} = 95.05 \frac{\text{kJ}}{\text{kg}}$

$\dot{W}_t = 0.1167 \frac{\text{kg}}{\text{s}} (99.56 - 95.05) \frac{\text{kJ}}{\text{kg}}$   
 $= 0.53 \text{ kW} < 0.5 \cdot 5.17 \Rightarrow \text{Not possible}$